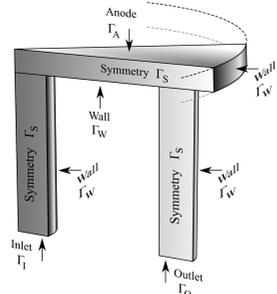
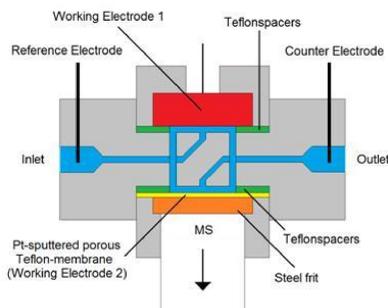


## Thin Layer Flow Cell

- Purpose: investigation of electrocatalytic surface reactions under controlled conditions using reasonably small electrolyte volumes
- Coupling to on-line product analysis by differential electrochemical mass spectrometry



Side view of 1/12 of the working chamber

## Inverse Modeling

- Result of experimental work: electrical and mass-spectrometry currents for given flow rates and inlet concentrations
- Aim: detection of inlet concentrations, species diffusion coefficients and reaction rates from measurements
- Interpretation of measurement data:
  - State of the art: auxiliary measurements with known characteristics to derive characteristic geometry coefficients
  - Project aim: Precise numerical modeling + data detection by fit procedure

## Numerical Discretisation = Navier Stokes + Transport Equations

- Stationary solvent flow with velocity  $\vec{u}$ , pressure  $p$ , dynamic viscosity  $\eta$  and density  $\rho$  inside the flow cell is governed by the incompressible Navier-Stokes equations

$$-\eta \Delta \vec{u} + \rho (\vec{u} \cdot \nabla) \vec{u} + \nabla p = 0 \quad \text{in } \Omega, \quad \nabla \cdot \vec{u} = 0 \quad \text{in } \Omega$$

- Divergence-constraint: crucial for mass conservation  $\Rightarrow$  use divergence-free finite element methods (Scott-Vogelius FEM, novel modified nonconforming Crouzeix-Raviart FEM [4]).
- Less expensive (non-divergence-free) Taylor-Hood FEM gives comparable results [2, 3].
- Species transport with concentration  $c$ , diffusion coefficient  $D$ :

$$\nabla \cdot (-D \nabla c + c \vec{u}_h) = s \quad \text{in } \Omega \quad \text{and} \quad c = c_{\text{in}} \quad \text{at inlet}$$

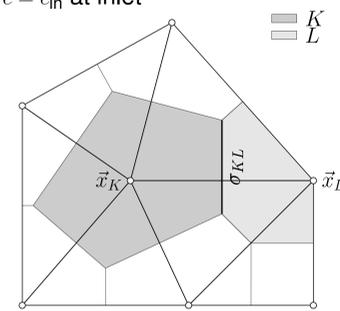
discretised by an exponentially fitted finite volume method with Voronoi cells as control volumes. On every  $\sigma_{KL} := \partial K \cap \partial L$  set

$$u_{\sigma_{KL}} := \int_{\sigma_{KL}} \vec{u}_h \cdot (\vec{x}_L - \vec{x}_K) ds / |\sigma_{KL}|$$

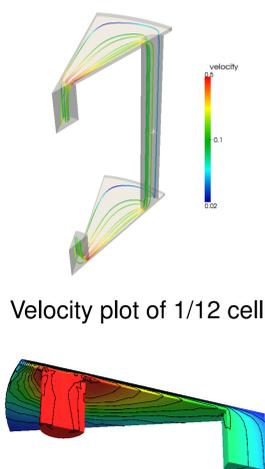
Find  $c_h \in P_0(\mathcal{K})$  with  $c_K := c_h|_K$  such that

$$\sum_{L \text{ neighbour of } K} |\sigma_{KL}| |\vec{x}_L - \vec{x}_K| g(c_K, c_L, u_{\sigma_{KL}}) = |K| s_K \quad \text{for all } K \in \mathcal{K}_0 := \mathcal{K} \setminus \mathcal{K}_D$$

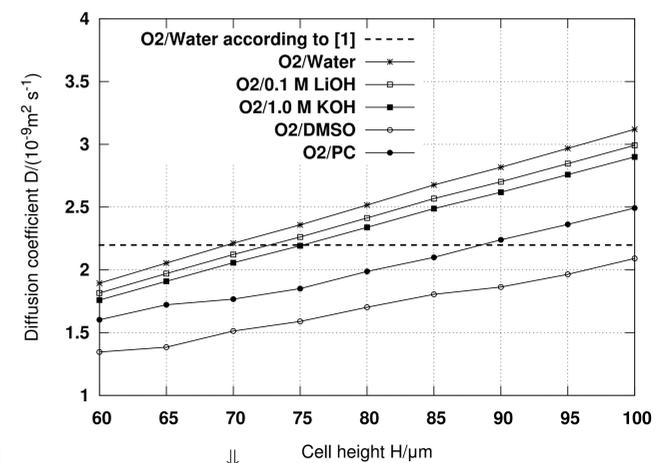
where  $g(c_K, c_L, u_{\sigma_{KL}}) := D(B(u_{\sigma_{KL}}/D)c_K - B(-u_{\sigma_{KL}}/D)c_L)$  with  $B(z) = z/(1 - e^{-z})$ .



## Detection of $O_2$ diffusion coefficients in various solvents



- Experiment:
  - Detection of relation between mass flow and mass spectrometric current by independent experiment
  - Detection of mass spectrometric current  $I$  from  $O_2$  diffusing through the membrane of the measurement chamber for flow rates  $u = 0.1 \dots 80 \text{ mm}^3/\text{s}$
- Interpretation:
  - Detection of inlet concentration from lowest flow rate under the assumption that no  $O_2$  remains in the outlet (strongly diffusion dominated case)
  - Levenberg-Marquardt fit of diffusion coefficient  $D$  using coupled flow+transport simulation as forward solver
  - Detection of working chamber height (uncertain due to experimental construction) based on known solvents ( $O_2/H_2O$ , [1])
  - Use fit procedure with known cell height to detect diffusion coefficient for new solvents



$$D_{O_2/0.1M \text{ LiOH}} = 2.12 \cdot 10^{-9} \text{ m}^2/\text{s} \quad D_{O_2/\text{DMSO}} = 1.51 \cdot 10^{-9} \text{ m}^2/\text{s}$$

$$D_{O_2/1.0M \text{ KOH}} = 2.06 \cdot 10^{-9} \text{ m}^2/\text{s} \quad D_{O_2/\text{PC}} = 1.77 \cdot 10^{-9} \text{ m}^2/\text{s}$$

## References

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